

Effects of Slip Velocity and Hall Currents on Peristaltic Transport of Bingham-Papanastasiou Fluid with Heat Transfer

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Abstract: In this paper, we study the effects of slip boundary condition and Hall currents on peristaltic motion of a non-Newtonian fluid which follows Bingham-Papanastasiou model, with heat transfer taking into account the thermal radiation and heat generation, through an asymmetric channel. This phenomena is modeled mathematically by a system of governing equations which are continuity, momentum and heat equations. These equations are solved analytically under low Reynolds number condition and long wavelength approximation. The stream function and temperature distribution are obtained as functions of physical parameters of the problem. The effects of the parameters on these solutions are discussed numerically and illustrated graphically through a set of figures. It is found that the physical parameters have important roles to control the velocity and temperature distribution.

Keywords: Slip boundary condition; Hall currents; Peristaltic transport; Bingham-Papanastasiou fluid model; Thermal radiation; Heat generation.

1 Introduction

The word peristalsis stems from the Greek word peristalikos. Peristalsis is defined as a wave of relaxation contraction (expansion) imparted by the walls of a flexible conduit, thereby pumping the enclosed material, it is a nature's way of moving the content within hollow muscular structures by successive contraction of their muscular fibers [1, 2, 3, 4]. Peristalsis is now well-known to the physiologists to be one of the major mechanisms for fluid transport in many biological systems, it results physiologically from neuron muscular properties of the tubular smooth muscles [5, 6].

The peristaltic transport may be involved in many biological organs, e.g., swelling food through the esophagus, movement of chime in the gastrointestinal tract, urine transport from the kidney to the bladder through the ureter, transport of spermatozoa in the ducts efferent of male reproduction tract and in the cervical canal of the female, movement of ova in the fallopian tub, vasomotion of small blood vessels such as venules and capillaries as well as blood flow in arteries, and in many

other glandular ducts [3, 4, 5, 6, 7]. There are also many industrial applications of the peristaltic transport like, blood pumps in heart lung machine, transport of corrosive fluid, where the contact of the fluid with the machinery parts is prohibited [4].

Although the majority of fluids in the biosphere have Newtonian behavior, non-Newtonian behavior is observed in most industrial synthetic and non-synthetic fluids and in biological fluids, such as human blood and saliva. To quote a few examples, crude oil and drilling muds from the oil industry, paints, cosmetics, glues, soaps, detergents and many food products. Among them, an important class of non-Newtonian materials presents a yield stress limit which must be exceeded before significant deformation can occur the so-called Viscoplastic materials. In order to model the stress-strain relation in these fluids, some fitting has been proposed such as the linear Bingham equation and the non-linear Herschel-Bulkley and Casson models [8, 9, 10].

On the other hand Viscoplastic fluids are characterized by the absence of deformations when the

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applied load is below a fixed threshold. Bingham fluids is a special class of Viscoplastic fluids named so after Bingham [11], who described several types of paint using this definition. Viscoplastic fluids constitute a very important class of non-Newtonian fluids. The modelling of Bingham materials is of crucial importance in industrial applications, since a large variety of materials (e.g. foams, pastes, slurries, oils, ceramics, etc.) exhibit the fundamental character of viscoplasticity, that is the capability of flowing only if the stress is above some critical value [12, 13, 14].

However, the Bingham model is not amenable to numerical analysis because in some complex applications, parts of material flow while the rest behaves as a solid. This causes difficulties in tracking the shape and the location of the yield surfaces and applying two different constitutive equations across them. In addition, at vanishing shear rates, the apparent viscosity in Bingham model becomes infinite, which leads to a discontinuity and numerical difficulties. To overcome these issues, Papanastasiou proposed a modified Bingham model to approximate the rheological behavior of Bingham type materials [15, 16, 17].

We are aware that the no-slip condition in fluid mechanics means that the fluid velocity matches the velocity of the solid boundary. Nearly 200 years ago Navier proposed in his original paper on linearly viscous fluids a general boundary condition that permits the possibility of slip at a solid boundary. This boundary condition assumes that the tangential velocity of the fluid relative to the solid at a point on its surface is proportional to the tangential stress acting at that point. The constant of proportionality between these two quantities may be termed a coefficient of sliding friction (the slip parameter), which is assumed to depend on the nature of the fluid and the solid surface [18]. Some experimental and theoretical studies stated that slip condition could not be ruled out as an important element to understanding of certain characteristic flow [19].

The fluid flows in the presence of magnetic field has promising applications in engineering, chemistry, physics, the polymer industry and metallurgy. Some examples include controlling the rate of cooling, blood plasma, drying, evaporation at the surface of a water body, geothermal reservoirs, thermal insulation, enhanced oil recovery, cooling of nuclear reactors, bleeding reduction during surgeries, hyperthermia etc. Also under the influence of powerful applied magnetic fields the Hall effects in peristalsis cannot be ignored. In such case the applied magnetic field is powerful or collision frequency is small [20].

There are several studies of peristaltic transport with different fluids under the effect of different types of the external forces, as mentioned in [21] and see also, [22, 23, 24]. To the best of our knowledge, no investigation has been made yet to investigate the effect of slip velocity on peristaltic transport for Bingham-Papanastasiou fluid in the presence of Hall current and heat transfer.

In this article the vector form of the equations of motion of the non-Newtonian Bingham-Papanastasiou fluid as well as energy equation and the constitutive equations of that fluid are written in section 2. The formulation of the problem is introduced mathematically in section 3. In section 4 the stream, velocity and temperature distribution functions; which are calculated analytically and with the help of Mathematica program; are written. Results and discussion are explained in section 5 and the conclusion in section 6, this paper ends by the appendix and list of references.

2 Vector form of the problem's equations

The basic equations which describe the motion of non-Newtonian fluid with heat transfer can be written as

Continuity equation

$$\nabla \cdot \underline{V} = 0, \quad (1)$$

Momentum equation

$$\rho \frac{d\underline{V}}{dt} = -\nabla P + \nabla \cdot \underline{S} + \underline{J} \wedge \underline{B} \quad (2)$$

Energy equation

$$\rho c_p \frac{dT}{dt} = k_1 \nabla^2 T + \underline{S} \cdot \nabla \underline{V} - \nabla \cdot \underline{q}_r + Q(T - T_0), \quad (3)$$

where

$$\underline{J} = \sigma \left[(\underline{V} \wedge \underline{B}) - \frac{1}{e n_e} (\underline{J} \wedge \underline{B}) \right],$$

\underline{V} is fluid velocity vector, ρ is the density of the fluid, P is the pressure, \underline{S} is the extra-stress tensor (S_{ij}), \underline{J} is the current density vector including the Hall effect, σ is the electric conductivity, e is the electric charge, n_e is the number density of electrons, $\underline{B} = (0, 0, B_0)$ is the uniform magnetic field with magnetic flux density, T is temperature, k_1 is the thermal conductivity, $\frac{d}{dt}$ denotes the material time derivative and ∇^2 is the Laplacian operator, Q is heat generation, \underline{q}_r the radiation heat flux vector.

The regularized constitutive equation proposed by Papanastasiou [25] is

$$\underline{S} = \left[\mu + \frac{S_0(1 - \exp(-m\dot{\underline{\gamma}}))}{\dot{\underline{\gamma}}} \right] \dot{\underline{\gamma}}, \quad (4)$$

where μ is the plastic viscosity, S_0 is the yield stress, m is a stress growth exponent and $\dot{\underline{\gamma}}$ denotes the rate of strain tensor;

$$\dot{\underline{\gamma}} = \nabla \underline{V} + (\nabla \underline{V})^T \quad (5)$$

($\nabla \underline{V}$ is the velocity-gradient tensor and $(\nabla \underline{V})^T$ is its transpose) and $\dot{\gamma}$ is the magnitude of the rate of strain tensor,

$$\dot{\gamma} = |\dot{\underline{\gamma}}| = \sqrt{\frac{1}{2} II_{\dot{\underline{\gamma}}}} = \sqrt{\frac{1}{2} \dot{\underline{\gamma}} : \dot{\underline{\gamma}}} = \sqrt{\frac{1}{2} \sum_i \sum_j \dot{\gamma}_{ij} \dot{\gamma}_{ji}}, \quad (6)$$

where $II_{\dot{\underline{\gamma}}}$ is the second invariant of $\dot{\underline{\gamma}}$.

3 Mathematical formulation

Consider flow of fluid in two-dimensional asymmetric channel, X -axis is taken in motion direction while Y -axis is perpendicular on it and (U, V) are the velocity components in X and Y directions respectively as shown in Fig.(1).

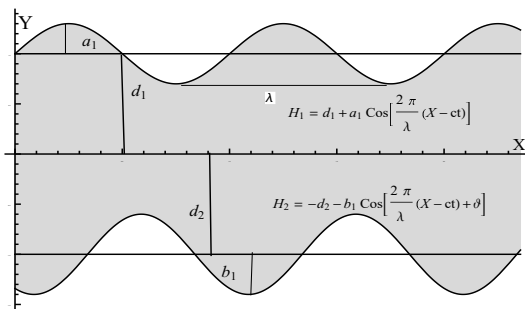


Fig. 1: The geometry of the problem.

The channel asymmetry is produced by choosing the peristaltic wave train on the walls to have different amplitudes and phase, consider the upper and lower channel walls are

$$Y = H_1 = d_1 + a_1 \cos \left[\frac{2\pi}{\lambda} (X - ct) \right] \quad (7)$$

$$Y = H_2 = -d_2 - b_1 \cos \left[\frac{2\pi}{\lambda} (X - ct) + \vartheta \right] \quad (8)$$

where a_1 and b_1 are the amplitudes of the waves, λ is the wavelength, $(d_1 + d_2)$ is the width of the channel and ϑ is the phase difference that varies in the range $0 \leq \vartheta \leq \pi$. Further, a_1, b_1, d_1, d_2 and ϑ satisfy the condition $a_1^2 + b_1^2 + 2a_1b_1 \cos \vartheta \leq (d_1 + d_2)^2$.

Introducing a wave frame (x, y) moving with the velocity c away from the laboratory frame (X, Y) , by the transformations

$$x = X - ct, \quad y = Y, \quad u = U - c, \quad v = V, \quad p(x) = P(X, t), \quad (9)$$

where u and v are the fluid velocity components and p is pressure in the wave frame of references.

Equations (1-3) will be on the form

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \quad (10)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial P}{\partial x} + \frac{\partial S_{xx}}{\partial x} + \frac{\partial S_{xy}}{\partial y} + \frac{\sigma B_0^2}{1 + \mathbf{H}^2} (\mathbf{H}v - (u + c)), \quad (11)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial P}{\partial y} + \frac{\partial S_{yx}}{\partial x} + \frac{\partial S_{yy}}{\partial y} - \frac{\sigma B_0^2}{1 + \mathbf{H}^2} (v + \mathbf{H}(u + c)), \quad (12)$$

$$\begin{aligned} \rho c_p \left(u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) &= k_1 \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) + S_{xx} \frac{\partial u}{\partial x} + \\ S_{xy} \frac{\partial u}{\partial y} + S_{yx} \frac{\partial v}{\partial x} + S_{yy} \frac{\partial v}{\partial y} - \frac{\partial q_r}{\partial y} + Q(T - T_0), \end{aligned} \quad (13)$$

where $\mathbf{H} = \frac{\sigma B_0}{e n_e}$ is the Hall parameter and the radiative heat flux in the X - direction is considered as negligible compared to Y - direction.

Also, the constitutive equations become

$$S_{xx} = 2 \left(\mu + \frac{S_0}{\dot{\gamma}} (1 - e^{-m\dot{\gamma}}) \right) \frac{\partial u}{\partial x}, \quad (14)$$

$$S_{xy} = S_{yx} = \left(\mu + \frac{S_0}{\dot{\gamma}} (1 - e^{-m\dot{\gamma}}) \right) \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right), \quad (15)$$

$$S_{yy} = 2 \left(\mu + \frac{S_0}{\dot{\gamma}} (1 - e^{-m\dot{\gamma}}) \right) \frac{\partial v}{\partial y}, \quad (16)$$

with

$$\dot{\gamma} = \left[2 \left(\frac{\partial u}{\partial x} \right)^2 + \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)^2 + 2 \left(\frac{\partial v}{\partial y} \right)^2 \right]^{\frac{1}{2}}, \quad (17)$$

and the wall equations will be

$$y = d_1 + a_1 \cos \frac{2\pi}{\lambda} x \quad (18)$$

$$y = -d_2 - b_1 \cos \left[\frac{2\pi}{\lambda} x + \vartheta \right]. \quad (19)$$

Further, by using Rosseland approximation for radiation, the radiative heat flux q_r is given by

$$q_r = -\frac{4}{3} \frac{\sigma_0}{k_0} \frac{\partial T^4}{\partial Y}$$

where σ_0 is Stefan-Boltzman constant and k_0 is the Rosseland mean absorption coefficient.

Moreover, we suppose that the temperature difference within the flow is sufficiently small such that T^4 may be expanded in a Taylor series. Hence, expanding T^4 about T_0 and ignoring higher order terms we get:

$$T^4 \cong 4 T_0^3 T - 3 T_0^4$$

i.e

$$q_r = -\frac{16 \sigma_0 T_0^3}{3 k_0} \frac{\partial T}{\partial Y} \quad (20)$$

Now introducing the stream function ψ ($u = \frac{\partial \psi}{\partial y}$, $v = -\frac{\partial \psi}{\partial x}$) and the following non-dimensional variables

$$\bar{x} = \frac{x}{\lambda}, \bar{y} = \frac{y}{d_1}, \delta = \frac{d_1}{\lambda}, \bar{u} = \frac{u}{c}, \bar{v} = \frac{v}{\delta c}, \bar{t} = \frac{c t}{\lambda}, a = \frac{a_1}{d_1},$$

$$b = \frac{b_1}{d_1}, d = \frac{d_2}{d_1}, h_1 = \frac{H_1}{d_1}, h_2 = \frac{H_2}{d_1}, \bar{\psi} = \frac{\psi}{c d_1}, \bar{s} = \frac{d}{\mu c} S$$

$$\bar{\gamma} = \frac{d_1 \dot{\gamma}}{c}, \bar{p} = \frac{d_1^2 p}{\mu \lambda c}, R = \frac{\rho c d_1}{\mu}, \mathcal{H} = \frac{\sigma B_0^2 d_1^2}{\mu}, \Theta = \frac{T - T_0}{T_w - T_0}, \quad (21)$$

after dropping bars and under the assumptions of long wavelength ($\delta \ll 1$) and low Reynolds number, the equation of continuity is simply verified.

Equations (11 - 13), using equation (20), become

$$-\frac{\partial p}{\partial x} + \frac{\partial S_{xy}}{\partial y} - \mathcal{H}^2 \left(\frac{\partial \psi}{\partial y} + 1 \right) = 0 \quad (22)$$

$$\frac{\partial p}{\partial y} = 0, \quad (23)$$

$$\left(1 + \frac{4}{3R_n} \right) \frac{\partial^2 \Theta}{\partial y^2} + P_r G \Theta + P_r E_c S_{xy} \frac{\partial^2 \psi}{\partial y^2} = 0, \quad (24)$$

Also, equations (14 - 17) become

$$S_{xx} = 0 \quad (25)$$

$$S_{xy} = \left[1 + \frac{B_n}{|\dot{\gamma}|} \left(1 - e^{-M|\dot{\gamma}|} \right) \right] \left(\frac{\partial^2 \psi}{\partial y^2} \right), \quad (26)$$

$$S_{yy} = 0 \quad (27)$$

$$|\dot{\gamma}| = \frac{\partial^2 \psi}{\partial y^2}. \quad (28)$$

So we can write

$$S_{xy} = \left[1 + \frac{B_n}{|\dot{\gamma}|} \left(1 - e^{-M|\dot{\gamma}|} \right) \right] \frac{\partial^2 \psi}{\partial y^2} \quad (29)$$

and for small values of M we will get

$$S_{xy} = (1 + B_n M) \frac{\partial^2 \psi}{\partial y^2} \quad (30)$$

where $\mathcal{H}^2 = \frac{\mathcal{H}}{1 + \mathbf{H}^2}$, $E_c = \frac{\mu c^2}{k_1 \Delta T} = \frac{c^2}{c_p \Delta T}$ is the Eckert number, $B_n = \frac{d_1}{\mu c} S_0$ is Bingham number, $M = \frac{c m}{d_1}$ is the dimensionless stress growth exponent, $P_r = \frac{\mu C_p}{k_1}$ is the Prandtl number, $R_n = \frac{k_1 k_0}{4 \sigma_0 T_0^3}$ is the radiation parameter, $G = \frac{Q d_1^2}{\mu C_p}$ is the generation parameter.

Equation (23) implies that $p \neq p(y)$, so we can write equation (24) after using (30) on the form

$$\left[\frac{\partial^2}{\partial y^2} - \frac{\mathcal{H}^2}{(1 + B_n M)} \right] \frac{\partial^2 \psi}{\partial y^2} = 0 \quad (31)$$

also, equation (24) will take the form

$$\left(1 + \frac{4}{3R_n} \right) \frac{\partial^2 \Theta}{\partial y^2} + P_r G \Theta + P_r E_c (1 + B_n M) \left(\frac{\partial^2 \psi}{\partial y^2} \right)^2 = 0 \quad (32)$$

It is obvious that when $B_n = 0$ equations (31) and (32) will represent the equations of motion and energy of ordinary Newtonian fluid.

Furthermore, the upper and lower channel walls in dimensionless forms will be

$$y = h_1 = 1 + a \cos 2\pi x, \quad (33)$$

$$y = h_2 = -d - b (\cos 2\pi x + \vartheta). \quad (34)$$

Also, the non-dimensional appropriate boundary conditions will be

$$\psi = \frac{q}{2}, \quad \frac{\partial \psi}{\partial y} + \beta \frac{\partial^2 \psi}{\partial y^2} = -1, \quad \Theta = 1, \quad \text{at } y = h_1, \quad (35)$$

$$\psi = -\frac{q}{2}, \quad \frac{\partial \psi}{\partial y} - \beta \frac{\partial^2 \psi}{\partial y^2} = -1, \quad \Theta = 0, \quad \text{at } y = h_2, \quad (36)$$

where q is the flux between the two walls in the wave frame and β is the non-dimensional slip parameter.

q is related to the dimensionless average volume flow rate over one period $T = \frac{\lambda}{c}$ of the peristaltic wave in the laboratory frame \bar{Q} through the relation $\bar{Q} = q + d + 1$.

Also, by integrating the axial pressure gradient $\frac{dp}{dx}$ over one wavelength λ , the pressure rise is given by the relation

$$\Delta p = \int_0^{\lambda} \frac{dp}{dx} dx \quad (37)$$

4 The proposed solution of the problem

Through introducing the boundary conditions (35 - 36) into (31, 32) the stream function will be

$$\psi = [l_7 (h_1 + h_2 - 2y) + 2 (l_8 \sinh \alpha (y - h_1) + l_9 \cosh \alpha (y - h_1) + h_1 - 2y) + 2 (l_{10} \sinh \alpha (y - h_2) + l_{11} \cosh \alpha (y - h_2) - h_2)] l_{12}$$

so the velocity in x -direction will be

$$u = [-2l_7 + 2(l_8\alpha \cosh \alpha (y - h_1) + l_9\alpha \sinh \alpha (y - h_1) - 2) + 2(l_{10}\alpha \cosh \alpha (y - h_2) + l_{11}\alpha \sinh \alpha (y - h_2))]l_{12}$$

and the temperature distribution equation will be

$$\Theta = l_{14}(\alpha^4 K^2 E_c l_{11}^2 (3R_n(4\alpha^2 - GP_r \times (\cosh \alpha(-h_1 - h_2 + 2y) - 1)) + 16\alpha^2)) + A_1 \sinh(\zeta y) + A_2 \cosh(\zeta y)$$

Where $\alpha, \zeta, l_1 - l_{14}, A_1$ and A_2 are given in the Appendix.

5 Results and discussion

In this section, we have presented a set of Figures (2-21), that describe qualitatively the effects of various parameters of interest on flow quantities such as the axial velocity u , axial pressure gradient $\frac{dp}{dx}$, pressure rise per wavelength ΔP , temperature distribution Θ .

Figs. (2-5) illustrate the variation of axial pressure gradient $\frac{dp}{dx}$ with x for different values of Bingham number B_n , slip parameter β and Hall parameter \mathbf{H} . The following results can be observed from these figures, the magnitude of the pressure gradient increases with increasing of B_n as shown in Fig. (2), while Figs. (3,4) showed that the magnitude of the pressure gradient decreases with increasing both of β and \mathbf{H} . It is also observed that the maximum pressure gradient occurs at the narrow part of the channel $x \simeq 0.42$, while in the special case of symmetric channel ($a=b, \vartheta = 0$) the narrow part at which the pressure gradient is maximum will be $x = 0.5$ (the middle of distance $x = 1$) as shown in Fig. (5) and that will be proved if we studied the effects of all parameters on $\frac{dp}{dx}$ for symmetric channel.

The effects of the phase angle ϑ, B_n, β and \mathbf{H} on the variation of the pressure rise ΔP with the average volume flow rate \bar{Q} are illustrated in Figs. (6-9). By looking at those figures, it is noticeable that ΔP has the maximum value when \bar{Q} is minimum and ΔP decreases until it has the minimum value when \bar{Q} is maximum. It is observed from Fig. (6) that the pressure rise decreases with the increasing of ϑ .

From Fig. (7), it is obvious that the pressure rise increases with B_n in region above a critical point (at which there no noticeable difference) and after that point it is obvious that the contrary occurs and ΔP decreases with the increasing in B_n .

Figs. (8,9) explain the effect of β and \mathbf{H} , it is clear that ΔP decreases with the increasing in β and \mathbf{H} in the region above a critical point and after that point we notice that ΔP increases with decreasing in β and \mathbf{H} .

Figs. (10-17) illustrate the effects of $B_n, \mathbf{H}, \beta, \vartheta$, Eckert number E_c , generation parameter G , Prandtel P_r

and radiation parameter R_n on the temperature Θ . In Figs. (10-16) we consider that $a = 0.5, b = 0.3, d = 0.5, x = 1, \vartheta = \frac{\pi}{2}$, i.e $h_1 = -1, h_2 = 1.5$. It is obvious that the temperature distribution satisfies our boundary conditions where $\Theta = 0$ at $y = h_1 = -1$ and $\Theta = 1$ at $y = h_2 = 1.5$. We observe that Θ increases with $B_n, E_c, G, \mathbf{H}, P_r$ and R_n as shown in Figs. (10-15). From Fig. (16) it is clear that Θ decreases in the increase of the slip parameter β .

Fig. (17) clarifies the effect of ϑ on the temperature distribution, it is obvious that Θ decreases with the increasing of ϑ . Also our boundary conditions on Θ are fulfilled where $\Theta = 1$ at $y = h_2 = 1.5$ for all values of ϑ and $\Theta = 0$: at $y = h_1 = -1.3$ when $\vartheta = 0$, at $y = h_1 \simeq -1.21$ when $\vartheta = \frac{\pi}{4}$ and at $y = h_1 = -1$ when $\vartheta = \frac{\pi}{2}$.

Figures (18-21) explain the effect of some parameters of the problem on the velocity distribution u . We observe that u increases with B_n, \mathbf{H} and ϑ as cleared through Figs. (18-20), while u decreases with increasing of the slip parameter β as illustrated in Fig. (21).

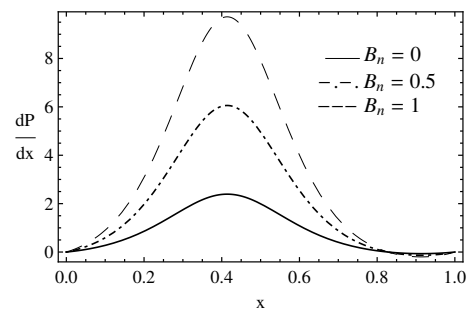


Fig. 2: The variation of the pressure gradient $\frac{dp}{dx}$ with x for several values of B_n when $a = 0.5, b = 0.3, d = 1, \vartheta = \frac{\pi}{2}, \bar{Q} = -0.5, \mathcal{K} = 1.2, \beta = 0.5, \mathbf{H} = 0.1, M = 5$.

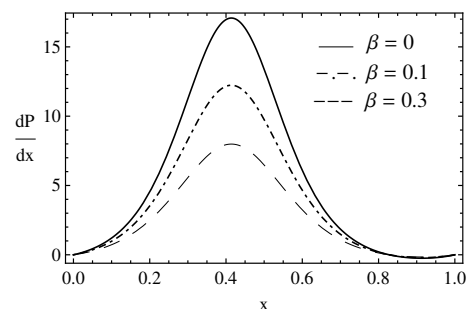


Fig. 3: The variation of the pressure gradient $\frac{dp}{dx}$ with x for several values of β when $a = 0.5, b = 0.3, d = 1, \vartheta = \frac{\pi}{2}, \bar{Q} = -0.5, \mathcal{K} = 1.2, B_n = 0.5, \mathbf{H} = 0.1, M = 5$.

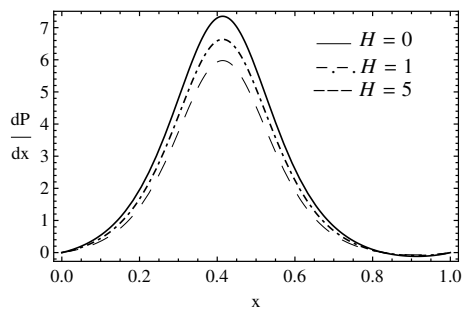


Fig. 4: The variation of the pressure gradient $\frac{dp}{dx}$ with x for several values of H when $a = 0.5$, $b = 0.3$, $d = 1$, $\vartheta = \frac{\pi}{2}$, $\bar{Q} = -0.5$, $\mathcal{H} = 1.2$, $\beta = 0.5$, $\mathbf{H} = 0.1$, $B_n = 0.5$, $M = 5$.

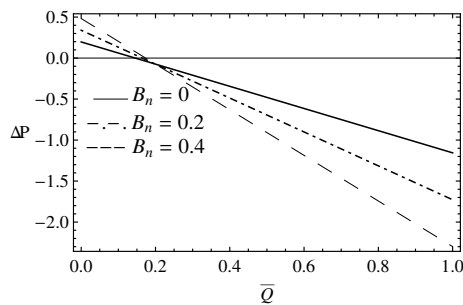


Fig. 7: The variation of the pressure rise ΔP with \bar{Q} for several values of B_n when $a = 0.5$, $b = 0.3$, $d = 1$, $\vartheta = \frac{\pi}{2}$, $\mathcal{H} = 1.2$, $\beta = 0.5$, $\mathbf{H} = 0.1$, $M = 5$.

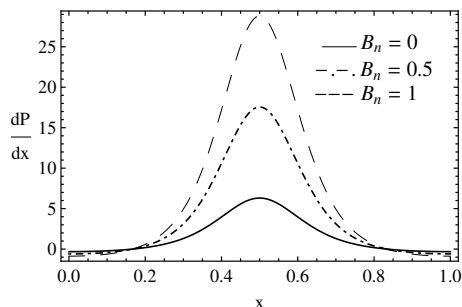


Fig. 5: The variation of the pressure gradient $\frac{dp}{dx}$ with x for several values of B_n when $a = 0.5$, $b = 0.5$, $d = 1$, $\vartheta = 0$, $\bar{Q} = -0.5$, $\mathcal{H} = 1.2$, $\beta = 0.5$, $\mathbf{H} = 0.1$, $M = 5$.

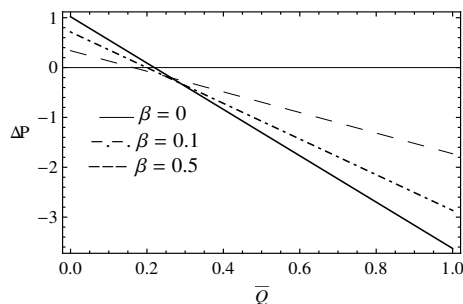


Fig. 8: The variation of the pressure rise ΔP with \bar{Q} for several values of β when $a = 0.5$, $b = 0.3$, $d = 1$, $\vartheta = \frac{\pi}{2}$, $\mathcal{H} = 1.2$, $\mathbf{H} = 0.1$, $B_n = 0.2$, $M = 5$.

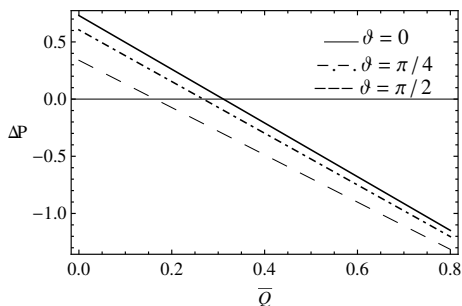


Fig. 6: The variation of the pressure rise ΔP with \bar{Q} for several values of ϑ when $a = 0.5$, $b = 0.3$, $d = 1$, $\mathcal{H} = 1.2$, $\beta = 0.5$, $\mathbf{H} = 0.1$, $B_n = 0.2$, $M = 5$.

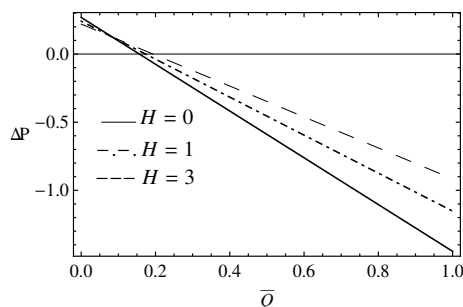


Fig. 9: The variation of the pressure rise ΔP with \bar{Q} for several values of \mathbf{H} when $a = 0.5$, $b = 0.3$, $d = 1$, $\vartheta = \frac{\pi}{2}$, $\mathcal{H} = 1.2$, $\beta = 0.5$, $B_n = 0.1$, $M = 5$.

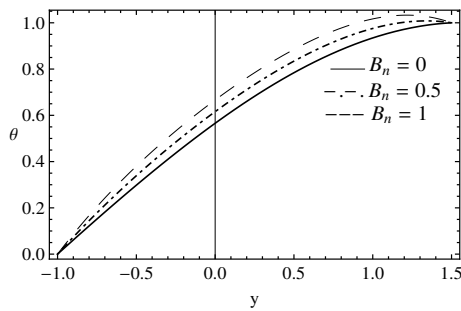


Fig. 10: The temperature distribution Θ is plotted against y for different values of Bingham number B_n when $a = 0.5, b = 0.3, d = 1, x = 1, \vartheta = \frac{\pi}{2}, q = 0.5, \mathcal{K} = 1.2, \beta = 0.5, \mathbf{H} = 0.1, M = 10, E_c = 0.1, Pr = 0.5, R_n = 3, G = 1$.

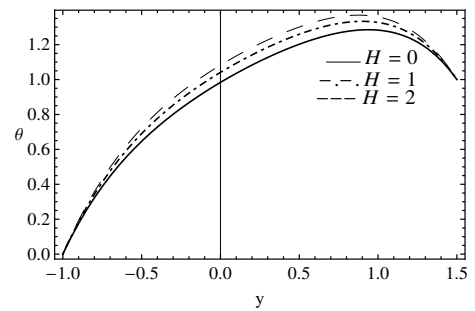


Fig. 13: The temperature distribution Θ is plotted against y for different values of Hall parameter \mathbf{H} when $a = 0.5, b = 0.3, d = 1, x = 1, \vartheta = \frac{\pi}{2}, q = 0.5, \mathcal{K} = 15, \beta = 0.5, E_c = 0.5, M = 10, B_n = 1, Pr = 0.5, R_n = 3, G = 1$.

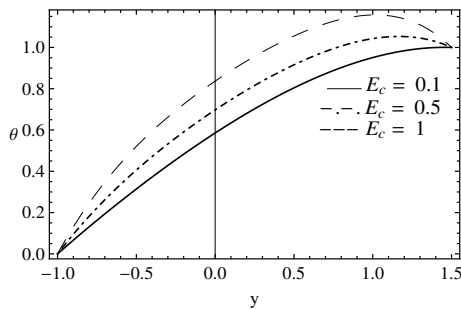


Fig. 11: The temperature distribution Θ is plotted against y for different values of Eckert number E_c when $a = 0.5, b = 0.3, d = 1, x = 1, \vartheta = \frac{\pi}{2}, q = 0.5, \mathcal{K} = 1.2, \beta = 0.5, \mathbf{H} = 0.1, M = 10, B_n = 0.2, Pr = 0.5, R_n = 3, G = 1$.

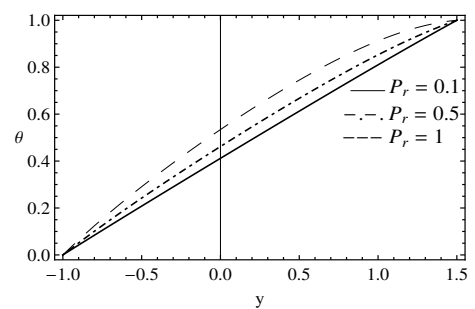


Fig. 14: The temperature distribution Θ is plotted against y for different values of the Prandtl number Pr when $a = 0.5, b = 0.3, d = 1, x = 1, q = 0.5, \vartheta = \frac{\pi}{2}, \mathcal{K} = 1.2, \beta = 0.5, E_c = 0.1, M = 10, \mathbf{H} = 0.1, B_n = 0.2, R_n = 3, G = 0.3$.

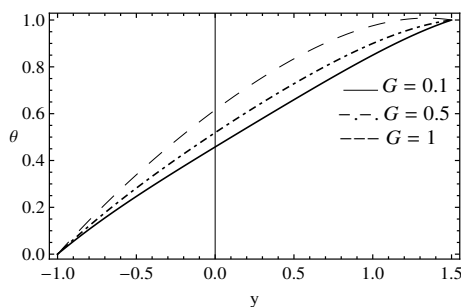


Fig. 12: The temperature distribution Θ is plotted against y for different values of heat generation parameter G when $a = 0.5, b = 0.3, d = 1, x = 1, \vartheta = \frac{\pi}{2}, q = 0.5, \mathcal{K} = 1.2, \beta = 0.5, \mathbf{H} = 0.1, M = 10, B_n = 0.5, Pr = 0.5, R_n = 3, E_c = 0.1$.

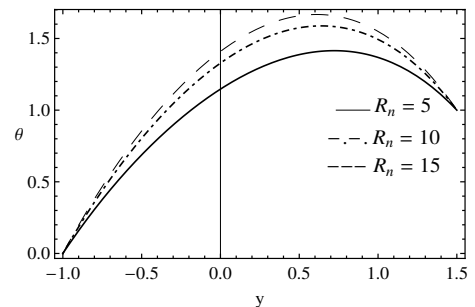


Fig. 15: The temperature distribution Θ is plotted against y for different values of the radiation parameter R_n when $a = 0.5, b = 0.3, d = 1, x = 1, q = 0.5, \vartheta = \frac{\pi}{2}, \mathcal{K} = 1.2, \beta = 0.5, E_c = 0.1, M = 10, \mathbf{H} = 0.1, B_n = 0.2, Pr = 3, G = 0.3$.

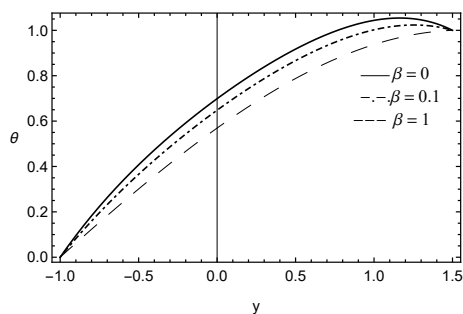


Fig. 16: The temperature distribution Θ is plotted against y for different values of the slip parameter β when $a = 0.5, b = 0.3, d = 1, x = 1, q = 0.5, \vartheta = \frac{\pi}{2}, \mathcal{K} = 1.2, R_n = 3, E_c = 0.1, M = 10, \mathbf{H} = 0.1, B_n = 1, P_r = 0.5, G = 1$

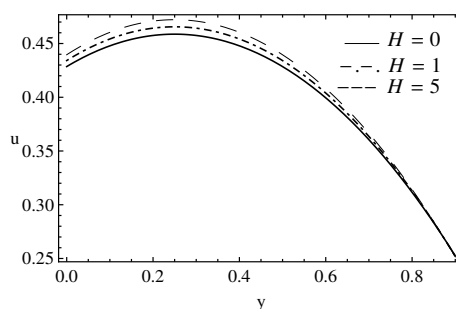


Fig. 19: The velocity u is plotted against y for different values of the Hall parameter \mathbf{H} when $a = 0.5, b = 0.3, d = 1, x = 1, q = 0.5, \vartheta = \frac{\pi}{2}, \beta = 0.5, \mathcal{K} = 1.2, M = 10, B_n = 0.2$

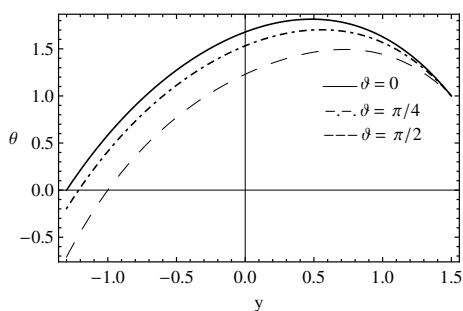


Fig. 17: The temperature distribution Θ is plotted against y for different values of the phase angle ϑ when $a = 0.5, b = 0.3, d = 1, x = 1, q = 0.5, \mathcal{K} = 1.2, \beta = 0.5, E_c = 0.1, M = 10, \mathbf{H} = 0.1, B_n = 0.5, P_r = 3, R_n = 3, G = 0.3$

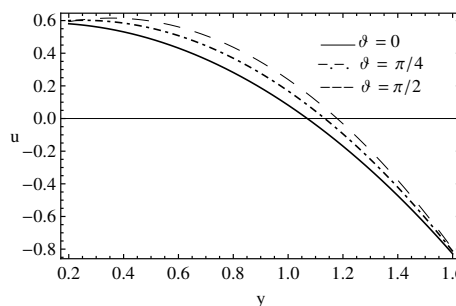


Fig. 20: The velocity u is plotted against y for different values of the phase angle ϑ when $a = 0.5, b = 0.3, d = 1, x = 1, q = 0.5, M = 10, \beta = 0.2, \mathcal{K} = 1.2, \mathbf{H} = .2, B_n = 5$

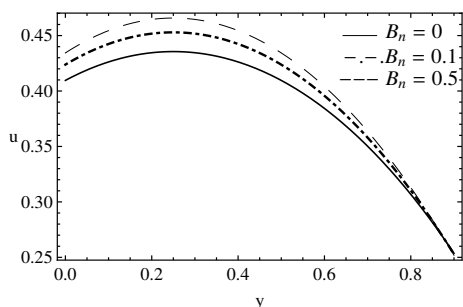


Fig. 18: The velocity u is plotted against y for different values of the Bingham number B_n when $a = 0.5, b = 0.3, d = 1, x = 1, q = 0.5, \vartheta = \frac{\pi}{2}, \beta = 0.5, \mathcal{K} = 1.2, M = 10, \mathbf{H} = 0.2$

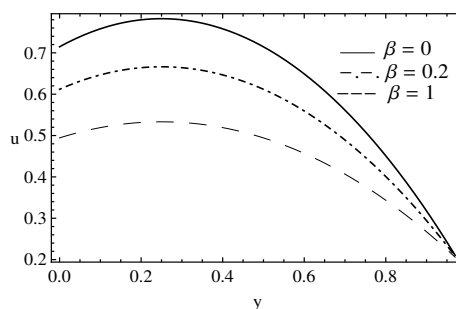


Fig. 21: The velocity u is plotted against y for different values of the slip parameter β when $a = 0.5, b = 0.3, d = 1, x = 1, q = 0.5, \vartheta = \frac{\pi}{2}, M = 10, \mathcal{K} = 1.2, \mathbf{H} = 1, B_n = 0.2$

6 Conclusion

The problem of two-dimensional peristaltic flow of a non-Newtonian Bingham-Papanastasiou fluid with heat transfer, through asymmetric channel, under the influence of slip boundary condition and Hall currents is formed. The equations governing this motion have been solved analytically under the conditions of low Reynolds number and long wavelength approximations, subjected to a set of appropriate boundary conditions. The expressions of velocity and temperature distribution have been evaluated for different parameters and have been shown graphically through a set of figures. The very important results can be summarized as following:

- 1-the pressure gradient has the maximum value at $x \approx 0.42$.
- 2-the pressure rise is maximum if the flow rate is minimum while it be minimum if the flow rate is maximum.
- 3-the temperature distribution increases with $B_n, \mathbf{H}, E_c, G, P_r$ and R_n while it decreases with the increasing of β and ϑ .
- 4-the velocity increases with B_n, \mathbf{H} and ϑ while it decreases with the increasing of the β .

Appendix

$$\alpha = \frac{\mathcal{H}}{\sqrt{(1+B_nM)}}, \quad \zeta = \sqrt{\frac{3GR_nPr}{-3R_n-4}}, \quad l_1 = \frac{\alpha}{2} (h_1 - h_2),$$

$$l_2 = 2\alpha ((h_1 - h_2) (\alpha^2\beta^2 + 1) - 2\beta),$$

$$l_3 = \frac{4(\alpha^2\beta(h_1 - h_2) - 1)}{l_2 \sinh 2l_1 + l_3 \cosh 2l_1 + 4}, \quad l_5 = -\alpha(q\alpha^2\beta^2 + 2\beta + q), \quad l_6 = -2(q\alpha^2\beta + 1),$$

$$l_7 = \frac{l_5 \sinh 2l_1 + l_6 \cosh 2l_1}{- \alpha\beta(h_1 + h_2 + q)}, \quad l_9 = (h_1 + h_2 + q),$$

$$l_{10} = \alpha\beta(h_1 - h_2 + q),$$

$$l_{11} = (h_1 - h_2 + q), \quad l_{12} = \frac{1}{l_4}, \quad l_{14} = \frac{1}{l_{13}}, \quad l_{13} = 8G((\alpha\beta l_1 - 1) \sinh l_1 + l_1 \cosh l_1)^2 (3R_n(GPr + 4\alpha^2) + 16\alpha^2),$$

$$A_1 = l_{14}[\operatorname{cosech}(\zeta(h_1 - h_2))(\alpha^4 K^2 A_c l_{11}^2 (\cosh(h_1 \zeta) - \cosh(h_2 \zeta)) (3R_n(4\alpha^2 - GPr(\cosh(2l_1) - 1)) + 16\alpha^2) + l_{13} \cosh(h_2 \zeta)],$$

$$A_2 = -l_{14}[\operatorname{cosech}(\zeta(h_1 - h_2))(\alpha^4 K^2 A_c l_{11}^2 (\sinh(h_1 \zeta) + \sinh(h_2 \zeta)) (3R_n(4\alpha^2 - GPr(\cosh(-2l_1) - 1)) + 16\alpha^2) + l_{13} \sinh(h_2 \zeta)].$$

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